WASTEWATER MANAGEMENT IN THE 21ST CENTURY: ISSUES FOR THE DESIGN OF TREATMENT WETLANDS

> III Conferencia Panamericana de Sistemas de Humedales para el Tratamiento y Mejoramiento de la Calidad del Agua

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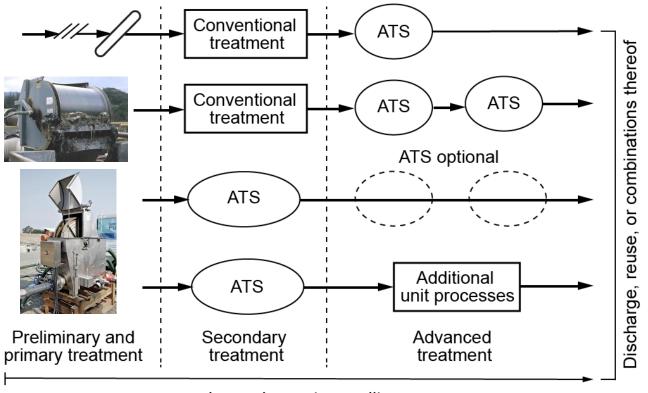
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TOPICS

- Use of aquatic treatment systems (ATS)
- Types of non and intensified treatment wetlands
- Paradigm shift in view of wastewater
- A fundamental question
- Wastewater management challenges
- Wastewater treatment opportunities
- The status of wetlands
- Modeling wetlands
- Intensified treatment wetland
- Closing thoughts

TYPICAL USES OF AQUATIC TREATMENT SYSTEMS (ATS) FOR WASTEWATER TREATMENT

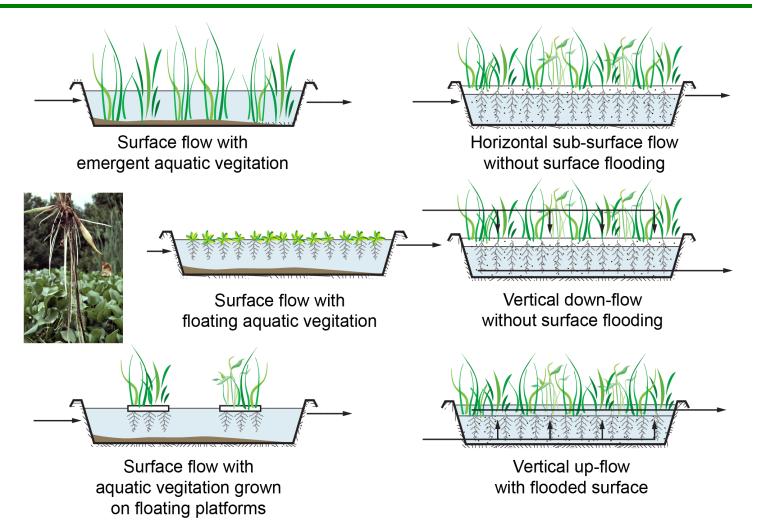


Improving water quality

TYPES OF NON-INTENSIFIED CONSTRUCTED TREATMENT WETLANDS

- Surface flow wetland with:
 - Emergent aquatic vegetation and open water zones
 - Free floating aquatic vegetation
 - Emergent aquatic vegetation grown on floating structures
 - Submerged aquatic vegetation
- Horizontal sub-surface flow wetland without surface flooding
- Vertical down-flow flow wetland without surface flooding
- Vertical up-flow flow wetland with flooded surface
- Fill and draw (tidal-flow) wetland

TYPES OF NON-INTENSIFIED CONSTRUCTED TREATMENT WETLANDS



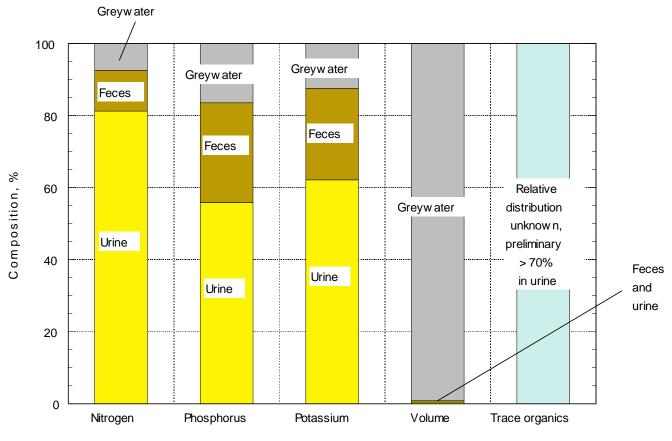
TYPES OF INTENSIFIED CONSTRUCTED TREATMENT WETLANDS

- Surface flow wetland with:
 - Alternative flow configurations with aeration and recycle
 - ^o Side stream oxygenation for nitrification
 - Side stream anammox reactor
 - P-binding enhanced (sub-charge neutralization dosing of alum or FeCl₃ dose)
- Horizontal sub-surface flow wetland without surface flooding with aeration
- Horizontal sub-surface flow anoxic wetland
- Vertical down- or up-flow flow wetlands with aeration
- Fill and draw (tidal-flow) wetland with:
 - ^o Single pass (high NH₄⁺ exchange capacity medium)
 - Recirculating (low NH_4^+ exchange capacity medium)

PARADIGM SHIFT IN VIEW OF WASTEWATER FOR THE 21ST CENTURY

WASTEWATER is a RENEWABLE RECOVERABLE SOURCE of POTABLE WATER, RESOURCES, and ENERGY

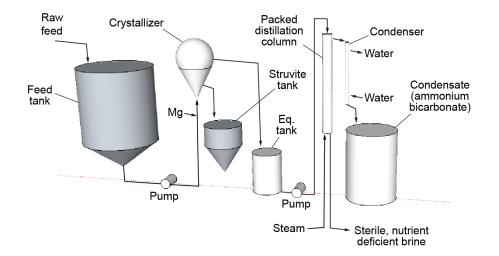
REMOVAL OF NUTRIENTS AND TRACE ORGANICS IN DOMESTIC WASTEWATER UPSTREAM REDUCES DOWNSTREAM TREATMENT REQUIREMENTS



Wastew ater constituent

Source: Jönsson et al.(2000) Recycling Source Separated Human Urine.

NUTRIENT RECOVERY FROM SOURCE SEPARATED URINE



Phosphate is recovered from urine as magnesium ammonium phosphate and/or magnesium potassium phosphate; nitrogen is recovered as ammonium bicarbonate



ENERGY CONTENT OF WASTEWATER CONSTITUENTS

Item	Unit	Range
Wastewater, heat basis	MJ/10°C•10 ³ m ³	41,816
Wastewater, COD basis	MJ/kg COD	12 - 16
Primary sludge, dry	MJ/kg TSS	15 - 15.9
Biosolids, dry	MJ/kg TSS	12.4 - 13.5

REQUIRED AND AVAILABLE ENERGY FOR WASTEWATER TREATMENT, EXCLUSIVE OF HEAT ENERGY

- Energy required for secondary wastewater treatment
 - 1,200 to 2,400 MJ/1000 m³
- Energy available in wastewater for treatment (assume COD = 500 g/m³) $Q = [500 \text{ kg COD}/1000 \text{ m}^3) (1000 \text{ m}^3) (13 \text{ MJ/ kg COD})$ = 6,000 MJ/1000 m³
- Energy available in wastewater is 2 to 4 times the amount required for treatment

A FUNDAMENTAL QUESTION

WHAT IS THE OPTIMAL USE OF THE CARBON IN WASTEWATER?

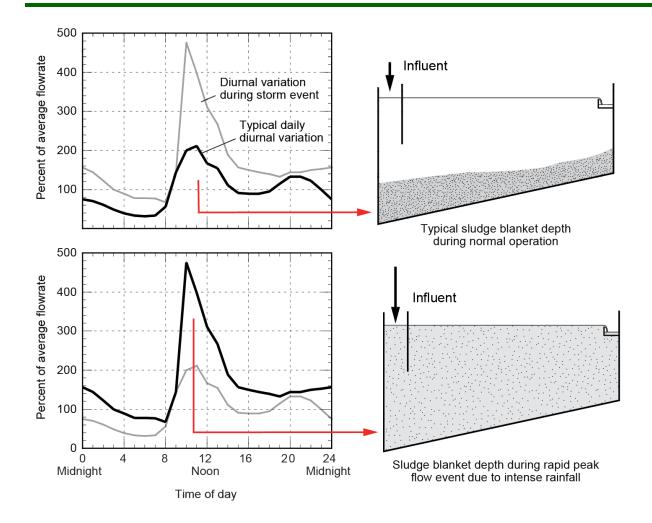
OPTIMAL USE OF CARBON IN WASTEWATER

Is the optimal use of the carbon in wastewater for **nitrogen removal, resource recovery** (e.g. fiber, organic polymers, etc.) or **energy production** or some combination?

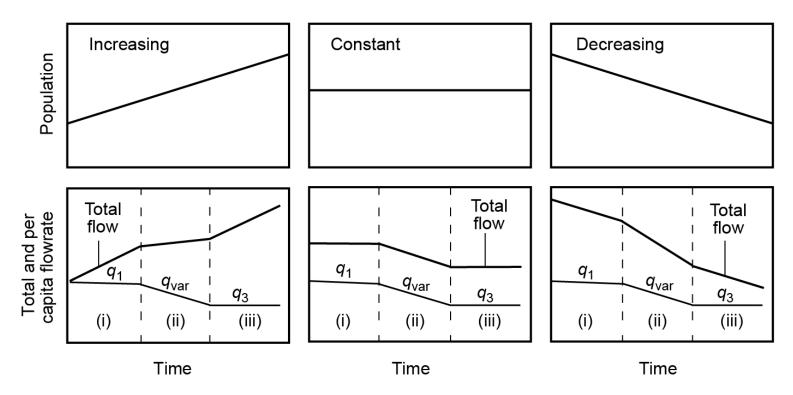
CHALLENGES AND ISSUES FOR WASTEWATER MANAGEMENT

- IMPACT OF CLIMATE CHANGE
- DECREASING PER CAPITA FLOWRATES

IMPACT OF CLIMATE CHANGE ON RAINFALL INTENSITY AND OPERATION OF WWTPS

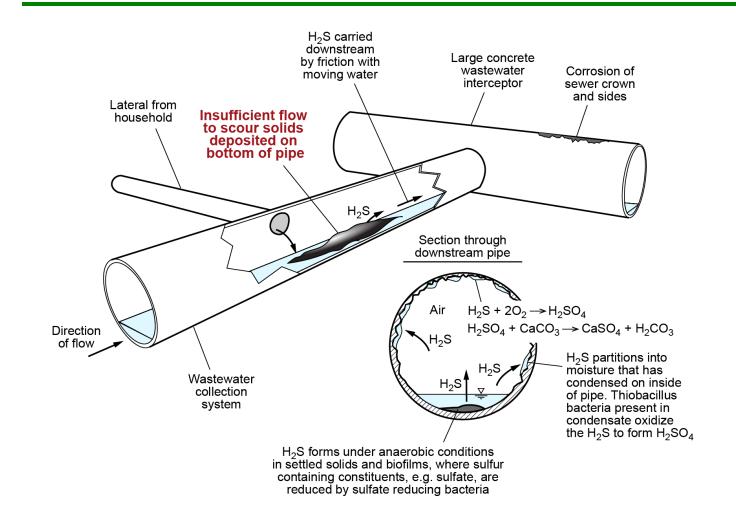


IMPACT OF DECREASING FLOWRATES ON OPERATION OF COLLECTION SYSTEMS AND WWTPs



- q = per capita wastewater flowrate
- (i) Pre-1992
- (ii) Improved water conservation, period end point unknown
- (iii) Maximum water conservation

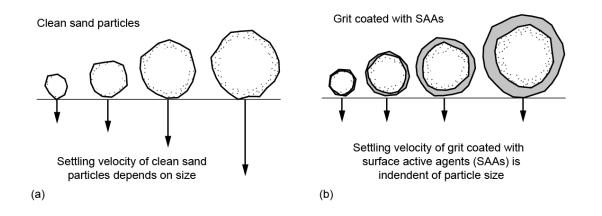
IMPACT OF WATER CONSERVATION AND DROUGHT: SOLIDS DEPOSITION, H₂S FORMATION, AND DOWNSTREAM CORROSION DUE TO REDUCED FLOWS

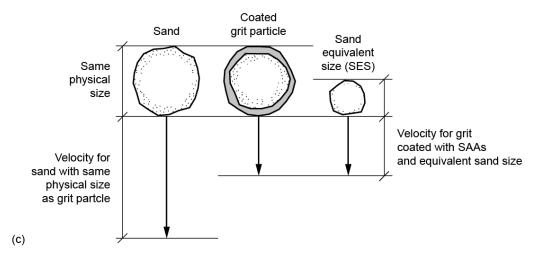


WASTEWATER TREATMENT: OPPORTUNITIES THAT WILL IMPACT THE DESIGN OF TREATMENT WETLANDS

- Enhanced preliminary treatment
- Alternative primary processes
- Altering the characteristics of wastewater
- Replace primary clarification facilities
- Design for alternative endpoint(s)

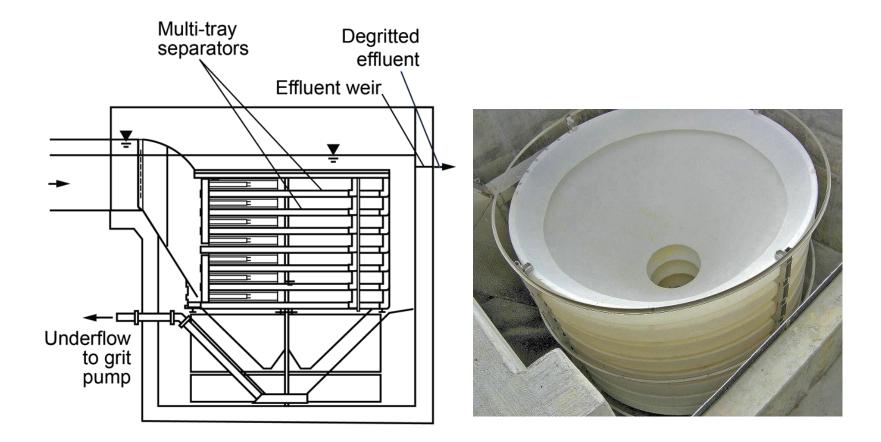
ENHANCED PRELIMINARY TREATMENT THROUGH BETTER CHARACTERIZATION OF GRIT



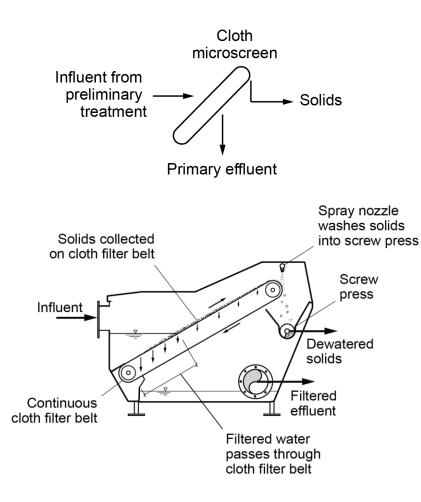


Source: Wastewater Engineering, 5th ed, McGraw-Hill, 2014

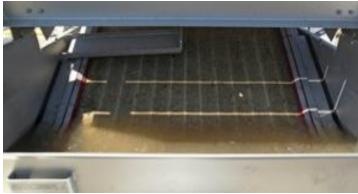
MULTI-TRAY GRIT SEPARATOR FOR ENHANCED GRIT REMOVAL



ALTERNATIVE TECHNOLOGIES FOR ENHANCED PRIMARY TREATMENT: CLOTH SCREEN (250-300 MM)

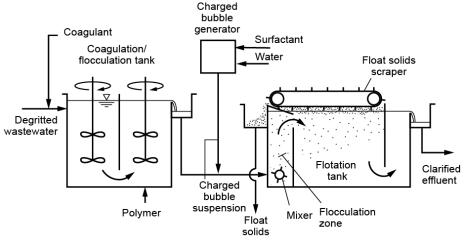






ALTERNATIVE TECHNOLOGIES FOR ENHANCED PRIMARY TREATMENT: CHARGED-BUBBLE FLOTATION

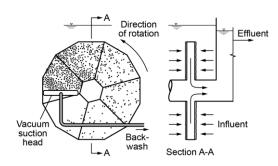






- 1/5th the size of conventional clarifiers
- Nanoparticles can be added to charged-bubble for removal of specific constituents

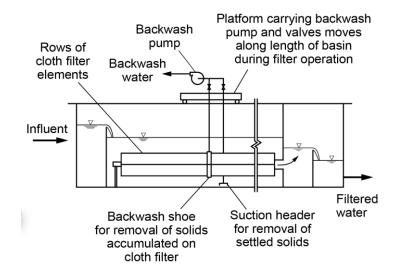
ALTERNATIVE TECHNOLOGIES FOR ENHANCED PRIMARY TREATMENT: CLOTH DISK FILTER (5-10 μm)





Vacuum suction head

Fiber thickness = 0.007 mmDepth filter L/D = 400 to 800Cloth filter L/D = 425 to 725



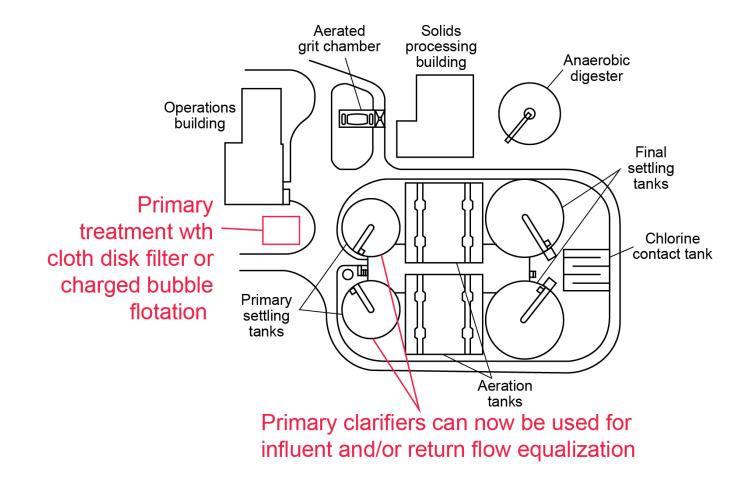
Parameter	Unit	Average influent	Average effluent	Average removal, %
BOD	mg/L	169	59	64.2
COD	mg/L	417	147	62.8
TSS	mg/L	221	26	87.5
VSS	mg/L	116	36	69.0
Turbidity	NTU	143	37	73.5
TKN	mg/L	39	36	7.7
FOG	mg/L	14	10	28.6
UVT	%	28	44	+59.9

ALTERING THE CHARACTERISTICS OF RAW WASTEWATER FOR ENHANCED DOWNSTREAM TREATMENT

KINETIC COEFFICIENTS BASED ON PARTICLE SIZE

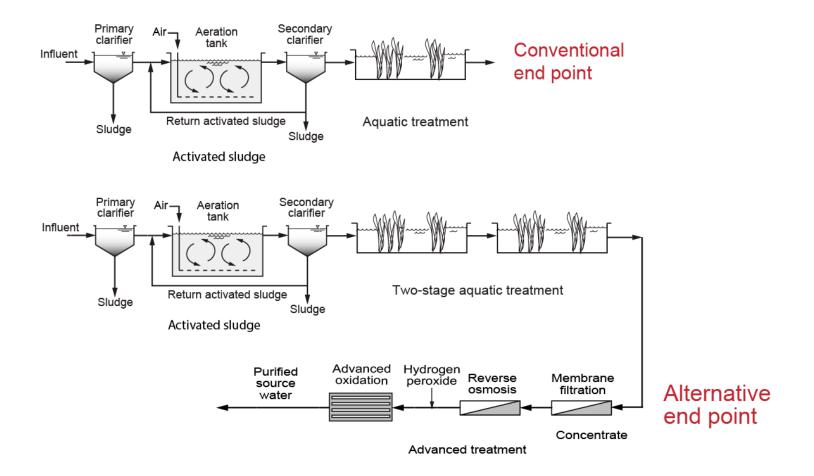
Fraction	Size range, μ	k (base 10), d-1
Settleable	> 100	0.08
Supracolloidal	1-100	0.09
Colloidal	0.1-1.0	0.22
Soluble	< 0.1	0.39

REPLACE AND REPURPOSE EXISTING PRIMARY CLARIFIERS



IN RESPONSE TO THE PARADIGM SHIFT, WASTEWATER TREATMENT PLANTS ARE BEING DESIGNED FOR ALTERNATIVE END USES

TREATMENT PROCESS DESIGN FOR ALTERNATIVE END POINT OR POINTS



THE STATUS OF WETLANDS IN WASTEWATER MANAGEMENT

- Both conventional and intensified wetlands have been used for the treatment of a variety of different wastes.
- New design variants are being developed, tested, and implemented continually.
- Although easy to construct, understanding the role of microorganisms and their consortia in wetlands is still in its infancy.
- As experience is gained, wetlands are also being considered as a unit processes.
- In many locations, stringent effluent discharge standards limit the use of conventional wetlands.

THE STATUS OF WETLANDS IN WASTEWATER MANAGEMENT

- Modeling of wetland systems is not well developed.
- To enhance their utility, the focus of wetland development is on process intensification, with special emphasis on improved wetland nitrification and TN removal.
- Phosphorus intensification is feasible and practical with micro-alum dosing.
- With passive intensification, zero to positive energy wastewater treatment may be possible.

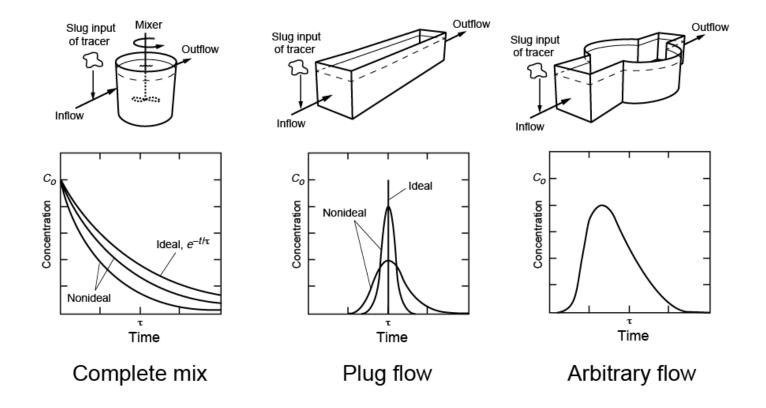
MODELING TREATMENT WETLAND SYSTEMS

- Must consider multiple removal and transformation mechanisms
- Wetland flow patterns
- Effect of particle size distribution
- Effect of sampling location
- Impact of short circuiting

PRINCIPAL REMOVAL AND/OR TRANSFORMATION MECHANISMS OCCURRING IN TREATMENT WETLANDS FOR THE CONSTITUENTS OF CONCERN IN WASTEWATER

Constituent	Removal and/or transformation mechanism
Biodegradable organics	Bioconversion by aerobic, facultative, and anaerobic bacteria on plant and debris surfaces of soluble BOD. Adsorption, filtration, and sedimentation of particulate BOD with subsequent bioconversion
Suspended solids	Sedimentation, filtration, adsorption, bioconversion
Nitrogen	Nitrification/denitrification (various pathways), deammonification, plant uptake, adsorption/volatilization
Phosphorus	Sedimentation, plant uptake, charge neutralization, chemical precipitation (induced with binding agents or naturally in hard water, high pH environment)
Heavy metals	Adsorption of plant and debris surfaces, sedimentation, chemical precipitation in sulfidic minerals
Trace organics	Volatilization, adsorption, UV irradiation, biodegradation (various biological pathways)
Pathogens	Natural decay, predation, UV irradiation, sedimentation, excretion of antibiotics from roots of plants

WETLAND FLOW PATTERNS



FLOW PATTERNS IN TREATMENT WETLANDS





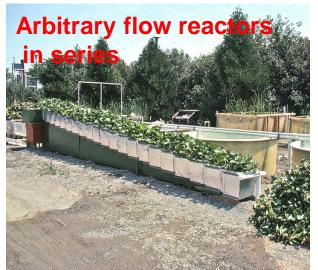
Arbitrary flow

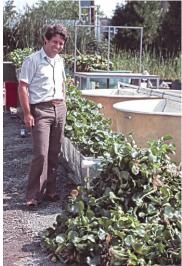




FLOW PATTERNS IN TREATMENT WETLANDS



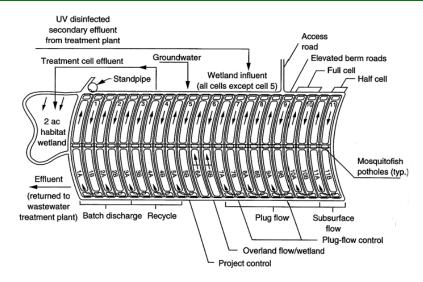








FLOW PATTERNS IN TREATMENT WETLANDS

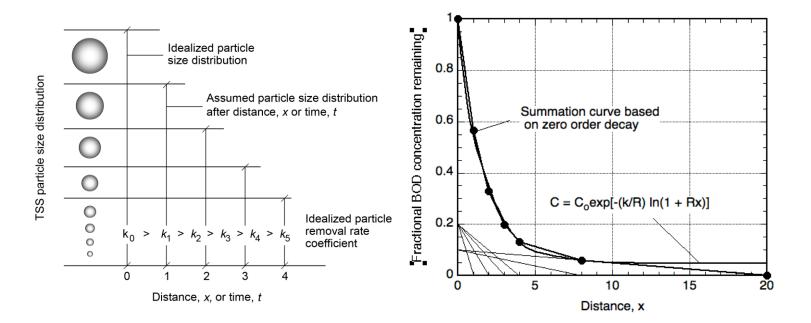








REMOVAL OF PARTICLATE MATTER AND BOD IN WASTEWATER IN WETLAND



REMOVAL RATE COEFFICIENT CANNOT BE CONSTANT!

MODELING TSS AND BOD REMOVAL

- Removal rate coefficient cannot be constant
- A retarded rate coefficient must be used. For example:

$$k_{apparent} = \frac{k_{o} (apparent)}{(1 + R_{X}x)^{n}} = \frac{k_{o} (apparent)}{(1 + R_{t}t)^{n}}$$
$$C = C_{o} \exp\left[-\frac{k}{R}\ln(1+Rt)\right] \quad (for n = 1)$$
$$C = C_{o} \exp\left[-\frac{k}{R(n-1)}\left(1 - \frac{1}{(1+Rt)^{n-1}}\right)\right] \quad (for n \neq 1)$$

VOLUME VERSUS AREA BASED COEFFIEICENTS

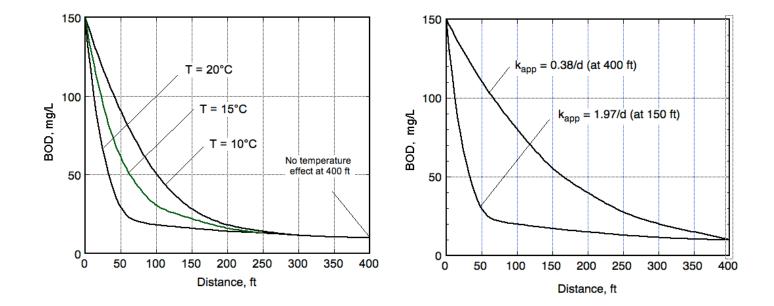
$$r_{BOD} = -k_v(BOD)^n$$

 k_v = volume based rate coefficient, 1/T

$$r_{BOD} = -k_A(A/V)(BOD)^n = -(k_A/H)(BOD)^n$$

 $k_A =$ area based rate coefficient, L/T
 $A =$ surface area, L²
 $V =$ volume, L³

EFFECT OF SAMPLING LOCATION



IMPACT OF SHORT CIRCUTING

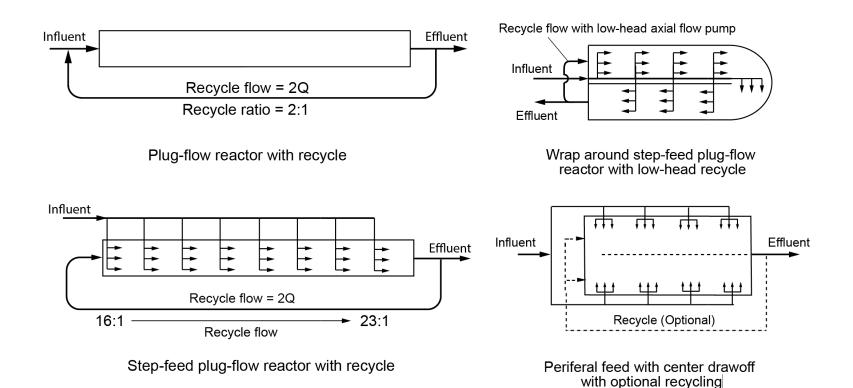


- Measured removal rate coefficients are *apparent* removal rate coefficients
- Most plug-flow wetlands can be modeled as a series of complete-mix reactors

INTENSIFICATION OF WETLAND TREATMENT

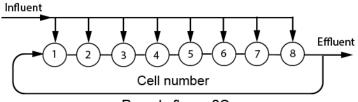
- Surface flow wetland with step-feed and recycle flow in linear or wrap around design
- Surface flow wetland with step-feed, aeration, and recycle flow
- Surface flow wetland with side-stream pure oxygen aeration
- Horizontal sub-surface flow aerated wetland
- Horizontal sub-surface flow anoxic wetland
- Tidal flow (fill and draw) reciprocating flow wetland
- Single pass high ammonia exchange capacity
- Surface flow with side-stream zeolite anammox treatment

INTENSIFICATION WITH STEP-FEED AND LOW-HEAD RECYCLE

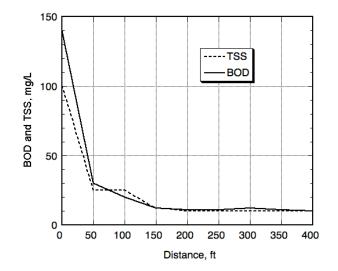


SURFACE FLOW WETLAND WITH STEP-FEED, AERATION, AND RECYCLE FLOW





Recycle flow = 2Q

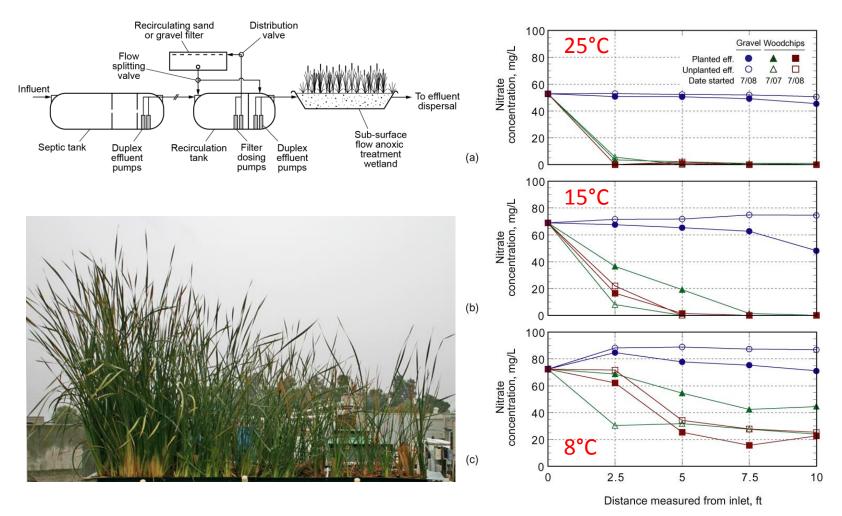


TYPICAL HORIZONTAL SUB-SURFACE FLOW AERATED WETLAND



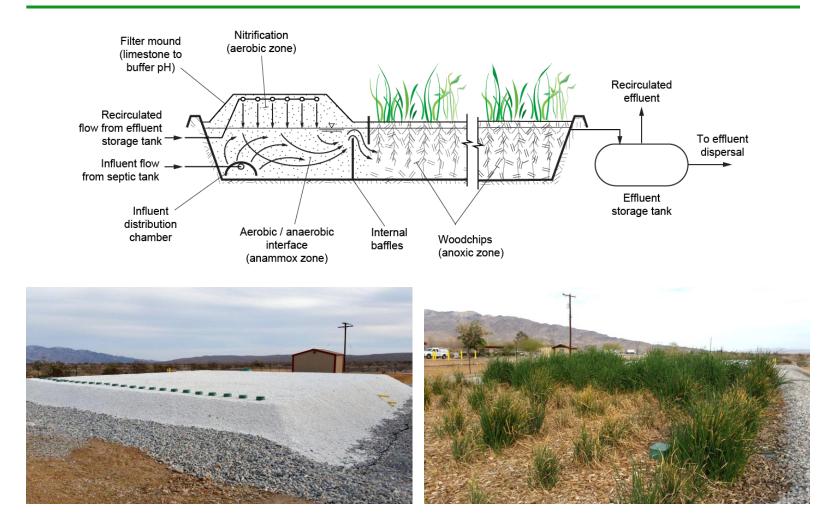
Courtesy David Austin, CH2M

HORIZONTAL SUB-SURFACE FLOW ANOXIC WETLAND FOR NITROGEN REMOVAL



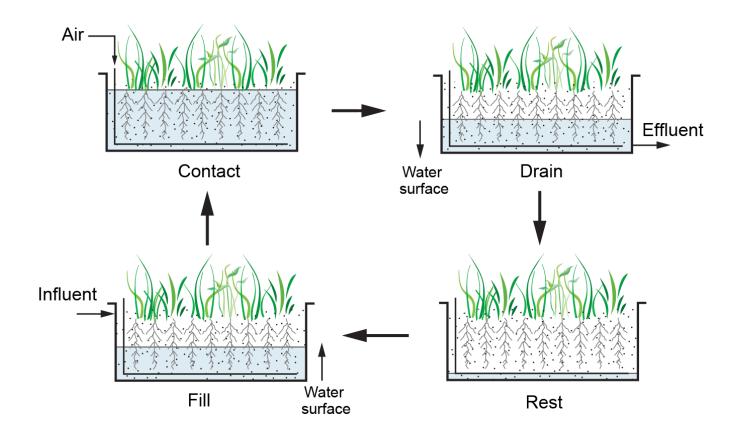
Courtesy Harold Leverenz

HORIZONTAL SUB-SURFACE FLOW ANOXIC WETLAND FOR NITROGEN REMOVAL

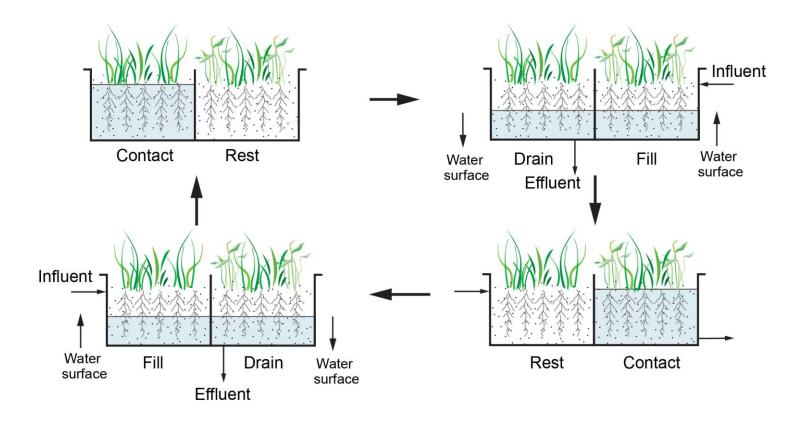


Courtesy Harold Leverenz

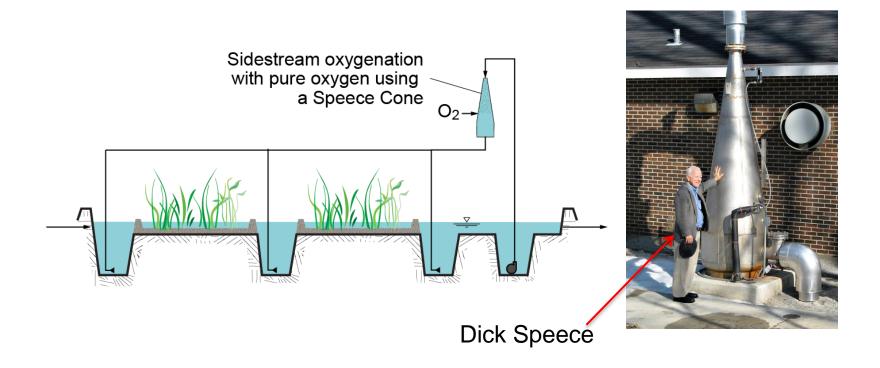
FILL AND DRAIN (TIDAL) WETLAND WITHOUT OR WITH AERATION



RECIPROCATING FILL AND DRAIN (TIDAL) WETLAND WITHOUT OR WITH AERATION AND ADSORPTIVE MEDIUM



SURFACE FLOW WETLAND WITH SIDESTREAM OXYGENATION FOR NITRIFICATION



TWO-STAGE FILL AND DRAIN (TIDAL) WETLAND WITH ADSORPTIVE MEDIM

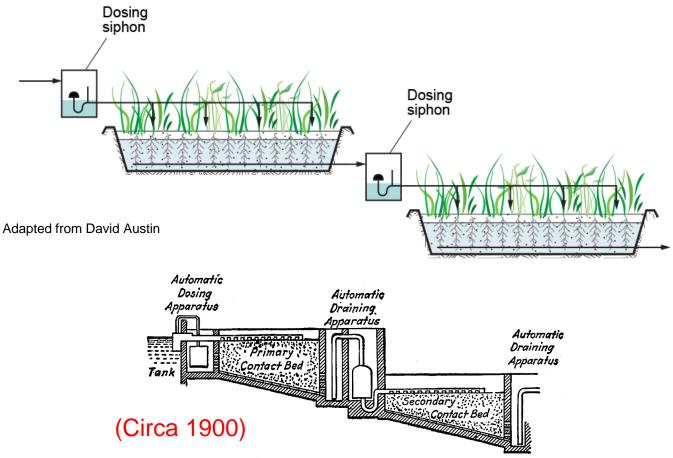


FIG. 115.—Arrangement of double contact beds.

SOME THOUGHTS ON WETLAND MODELING, INTENSIFICATION, AND UNKNOWNS

- While simple in concept, wetlands are complex from a process modeling standpoint.
- The intensification of wetlands will continue in response to more restrictive discharge requirements, land area constraints, and the need to reuse water
- Much remains to be known about the use of constructed wetlands for water quality improvement:

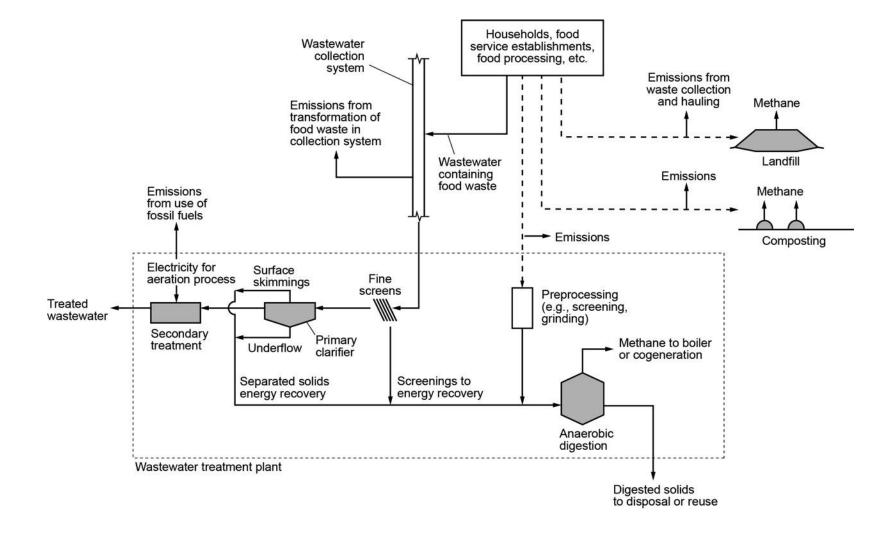
A CHALLENGE FOR ALLOF US!

CLOSING THOUGHT: A REMINDER

WASTEWATER is a RENEWABLE RECOVERABLE SOURCE of POTABLE WATER, RESOURCES, and ENERGY

THANK YOU FOR LISTENING

FOOD WASTE MANAGEMENT OPTIONS



CHARGED BUBBLE FLOTATION FOR ALGAL POND EFFLUENT REUSE



Algae dewatered on straw bed



Thickened algae ~4-5%

Effluent turbidity typically, <1 NTU



Pasteurization for disinfection Compressible medium effluent filtration